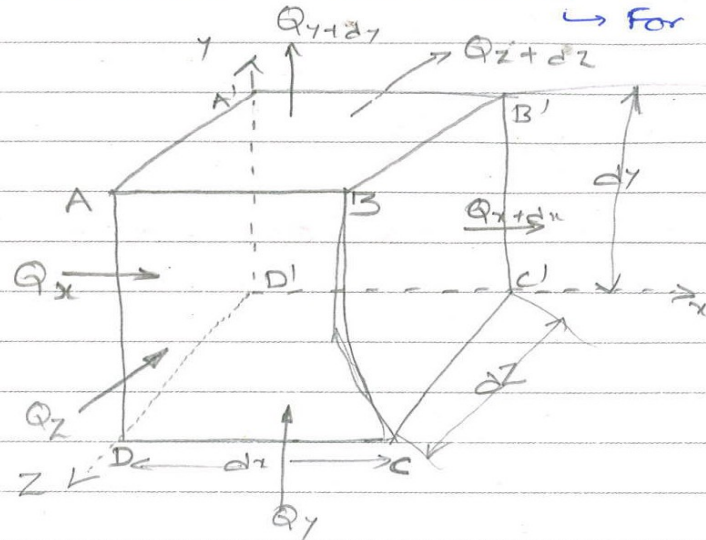


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# Heat Conduction through Cartesian, Cylindrical and Spherical Co-ordinates

- General Heat conduction equation:

(1) Cartesian Co-ordinates:



→ For solids with rectangular bodies like slabs, cubes etc.

Consider the flow of heat through an infinitesimal volume element oriented in 3D co-ordinate system.

The sides  $dx, dy, dz$  have been taken parallel to the  $x, y, z$  axis.

The energy balance for the little element as per 1<sup>st</sup> law of TD

Net heat conducted into element  $dx dy dz$  per unit time  $\left\{ \begin{array}{l} \textcircled{1} \\ + \\ \textcircled{2} \end{array} \right\} =$  Internal heat generated per unit time  $\textcircled{2}$

Increase in internal energy per unit time  $\left\{ \begin{array}{l} \textcircled{3} \\ + \\ \textcircled{4} \end{array} \right\} =$  work done by element per unit time  $\textcircled{4}$  —  $\textcircled{1}$

The quantity of heat flowing through  $AA'D'D'$  face during time interval  $dt$  is

$$\text{Heat influx } Q_x = -k_x \cdot (dy \cdot dz) \cdot \frac{dt}{dx} \cdot dt$$

$$\text{Heat outflux } Q_{x+dx} = Q_x + \frac{d}{dx}(Q_x) \cdot dx$$



Heat accumulated in  $x$ -direction

$$\begin{aligned}dQ_x &= Q_x - Q_{x+dx} \\ &= Q_x - (Q_x + \frac{\partial}{\partial x} \cdot Q_x \cdot dx) \\ &= -\frac{\partial}{\partial x} [k_x \cdot (dy \cdot dz) \cdot \frac{\partial T}{\partial x} \cdot dx] dx \\ &= -\frac{\partial}{\partial x} [k_x \cdot \frac{\partial T}{\partial x}] dx \cdot dy \cdot dz \cdot dx \quad \text{--- (2)}\end{aligned}$$

Similarly  $dQ_y = -\frac{\partial}{\partial y} [k_y \cdot \frac{\partial T}{\partial y}] dx \cdot dy \cdot dz \cdot dx \quad \text{--- (3)}$

Similarly  $dQ_z = -\frac{\partial}{\partial z} [k_z \cdot \frac{\partial T}{\partial z}] dx \cdot dy \cdot dz \cdot dx \quad \text{--- (4)}$

Total heat stored in the elemental volume due to heat flow along all axes is

$$\text{(2) + (3) + (4)} \\ \left[ -\frac{\partial}{\partial x} [k_x \cdot \frac{\partial T}{\partial x}] - \frac{\partial}{\partial y} [k_y \cdot \frac{\partial T}{\partial y}] - \frac{\partial}{\partial z} [k_z \cdot \frac{\partial T}{\partial z}] \right] dx \cdot dy \cdot dz \cdot dx \quad \text{--- (5)}$$

If  $q_g$  is heat generated per unit volume and per unit time then total heat generated in control volume =  $q_g \cdot dx \cdot dy \cdot dz \cdot dx \quad \text{--- (6)}$

Heat flow along Co-ordinate axes and heat generated in control volume increases thermal/internal energy of the lattice.

$$\text{Increase in thermal energy} = \rho \cdot (dx \cdot dy \cdot dz) \cdot C \cdot \frac{\partial T}{\partial t} \cdot dx \quad \text{--- (7)}$$

From energy balance considerations: (5) + (6) = (7)

$$\begin{aligned}& \left[ -\frac{\partial}{\partial x} (k_x \frac{\partial T}{\partial x}) - \frac{\partial}{\partial y} (k_y \frac{\partial T}{\partial y}) - \frac{\partial}{\partial z} (k_z \frac{\partial T}{\partial z}) \right] dx \cdot dy \cdot dz \cdot dx + q_g \cdot dx \cdot dy \cdot dz \cdot dx \\ &= \rho \cdot dx \cdot dy \cdot dz \cdot C \cdot \frac{\partial T}{\partial t} \cdot dx\end{aligned}$$

$$\frac{\partial}{\partial x} [k_x \cdot \frac{\partial T}{\partial x}] + \frac{\partial}{\partial y} [k_y \cdot \frac{\partial T}{\partial y}] + \frac{\partial}{\partial z} [k_z \cdot \frac{\partial T}{\partial z}] \neq q_g = \rho \cdot C \cdot \frac{\partial T}{\partial t}$$

↳ General heat conduction equation, establishes in differential form

the relationship between time & space variation of temperature at any point of the solid through which conduction takes place

$\rightarrow \rho, c, k$  are same everywhere in the material

- For homogeneous & isotropic material:

$\hookrightarrow$  These properties are not directional characteristics

Hence  $k_x = k_y = k_z = k$  then

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{q_g}{k} = \frac{\rho c}{k} \cdot \frac{\partial T}{\partial t} = \frac{1}{\alpha} \cdot \frac{\partial T}{\partial t}$$

$\rightarrow \alpha = k/\rho c$  is called Thermal diffusivity

$\hookrightarrow$  Tells how fast heat is propagated during changes of temp. with  $\alpha$  higher  $\Rightarrow$  Time required for heat to penetrate is shorter

$$\nabla^2 T + \frac{q_g}{k} = \frac{1}{\alpha} \cdot \frac{\partial T}{\partial t} \Rightarrow \text{Laplace equation}$$

- Special forms of heat conduction equation:

(i) Steady state:

There is no dependency of temp. on time.

Heat-flow equation 
$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{q_g}{k} = 0$$

$$\nabla^2 T + \frac{q_g}{k} = 0 \quad (\text{Poisson's equation})$$

(ii) In absence of internal heat generation

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} = 0$$

$$\nabla^2 T = 0 \quad (\text{Laplace equation})$$

(iii) Unsteady state with no internal heat generation

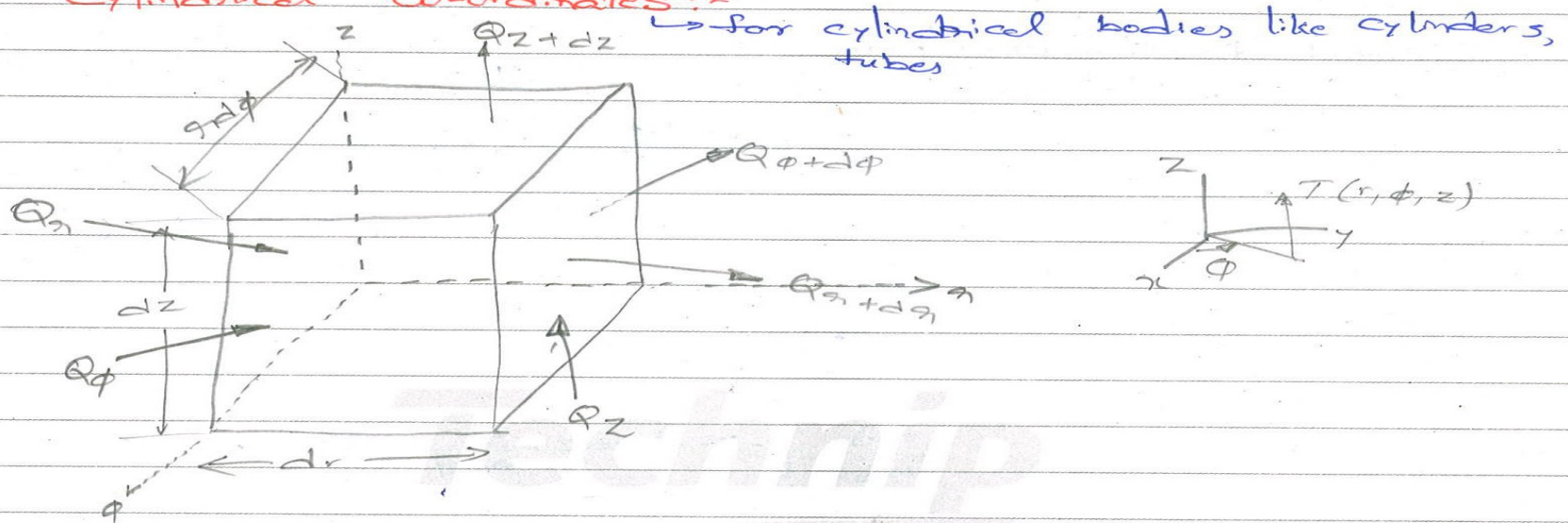
$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} = \frac{1}{\alpha} \cdot \frac{\partial T}{\partial t}$$

$$\nabla^2 T = \frac{1}{\alpha} \cdot \frac{\partial T}{\partial t} \quad (\text{Fourier equation})$$



iii) For one-D & steady state heat-flow with no internal heat generation, then  $\frac{d^2 T}{dx^2} = 0$

→ Cylindrical Co-ordinates :-



Consider a small volume element having sides  $dr, dz$  &  $r d\phi$  as shown in above fig.

Assuming material to be isotropic.

(i) radial direction ( $r-\phi$ ) plane :-

$$\text{Heat influx } Q_r = -k \cdot (r d\phi \cdot dz) \cdot \frac{\partial T}{\partial r} \cdot dr$$

$$\text{Heat efflux } Q_{r+dr} = Q_r + \frac{\partial}{\partial r} (Q_r) dr$$

Heat stored in the element due to flow of heat in radial direction

$$dQ_r = Q_r - Q_{r+dr}$$

$$= -\frac{\partial}{\partial r} (Q_r) dr$$

$$= -\frac{\partial}{\partial r} (-k \cdot (r d\phi \cdot dz) \cdot \frac{\partial T}{\partial r} \cdot dr) \cdot dr$$

$$\begin{aligned}
 &= k \cdot (dr \cdot d\phi \cdot dz) \frac{\partial}{\partial r} \left( r \cdot \frac{\partial t}{\partial r} \right) dr \\
 &= k \cdot dr \cdot d\phi \cdot dz \cdot \left[ r \cdot \frac{\partial^2 t}{\partial r^2} + \frac{\partial t}{\partial r} \right] dr \\
 &= k \cdot (dr \cdot r \cdot d\phi \cdot dz) \left[ \frac{\partial^2 t}{\partial r^2} + \frac{1}{r} \cdot \frac{\partial t}{\partial r} \right] dr
 \end{aligned}$$

(ii) Tangential direction (r-z plane)

$$\begin{aligned}
 \text{Heat influx } Q_\phi &= -k \cdot (dr \cdot dz) \cdot \frac{\partial t}{r \cdot d\phi} \cdot dr \\
 \text{Heat efflux } Q_{\phi+d\phi} &= Q_\phi + \frac{\partial}{\partial \phi} (Q_\phi) \cdot r \cdot d\phi
 \end{aligned}$$

Heat stored in tangential direction

$$\begin{aligned}
 dQ_\phi &= Q_\phi - Q_{\phi+d\phi} \\
 &= -\frac{\partial}{\partial \phi} (Q_\phi) \cdot r \cdot d\phi \\
 &= -\frac{\partial}{\partial \phi} \left[ -k \cdot dr \cdot dz \cdot \frac{\partial t}{r \cdot d\phi} \cdot dr \right] \cdot r \cdot d\phi \\
 &= k \cdot dr \cdot d\phi \cdot dz \cdot \frac{\partial}{\partial \phi} \left[ \frac{1}{r} \cdot \frac{\partial t}{\partial \phi} \right] \cdot dr \\
 &= k \cdot (dr \cdot r \cdot d\phi \cdot dz) \cdot \frac{1}{r^2} \cdot \frac{\partial^2 t}{\partial \phi^2} \cdot dr
 \end{aligned}$$

(iii) Axial direction (r-φ plane):

$$\begin{aligned}
 \text{Heat influx } Q_z &= -k \cdot (r \cdot d\phi \cdot dr) \cdot \frac{\partial t}{\partial z} \cdot dz \\
 \text{" efflux } Q_{z+dz} &= Q_z + \frac{\partial}{\partial z} (Q_z) \cdot dz
 \end{aligned}$$

Heat stored in the element due to heat flow in axial direction

$$\begin{aligned}
 dQ_z &= Q_z - Q_{z+dz} \\
 &= -\frac{\partial}{\partial z} \left[ -k \cdot (r \cdot d\phi \cdot dr) \cdot \frac{\partial t}{\partial z} \cdot dz \right] dz \\
 &= k \cdot (dr \cdot r \cdot d\phi \cdot dz) \frac{\partial^2 t}{\partial z^2} \cdot dz
 \end{aligned}$$



Heat generated within in control volume =  $q_g \cdot dv \cdot dz$

Rate of change of energy within in control volume =  $S \cdot dv \cdot c \cdot \frac{dT}{dz} \cdot dz$   
from energy equation

$$k \cdot dv \cdot \left[ \frac{d^2 T}{dz^2} + \frac{1}{r} \cdot \frac{dT}{dr} + \frac{1}{r^2} \cdot \frac{d^2 T}{d\phi^2} + \frac{d^2 T}{dz^2} \right] dz + q_g \cdot dv \cdot dz = S \cdot dv \cdot c \cdot \frac{dT}{dz} \cdot dz$$

Divide by  $dv \cdot dz$  on both sides

$$k \cdot \left[ \frac{d^2 T}{dz^2} + \frac{1}{r} \cdot \frac{dT}{dr} + \frac{1}{r^2} \cdot \frac{d^2 T}{d\phi^2} + \frac{d^2 T}{dz^2} \right] + q_g = S \cdot c \cdot \frac{dT}{dz}$$

$$\boxed{\left[ \frac{d^2 T}{dz^2} + \frac{1}{r} \cdot \frac{dT}{dr} + \frac{1}{r^2} \cdot \frac{d^2 T}{d\phi^2} + \frac{d^2 T}{dz^2} \right] + \frac{q_g}{k} = \frac{Sc}{k} \cdot \frac{dT}{dz} = \frac{1}{\alpha} \cdot \frac{dT}{dz}}$$

The heat conduction in cylindrical co-ordinates could also be obtained by doing following co-ordinate transformation

$$x = r \cos \phi \quad ; \quad y = r \sin \phi \quad ; \quad z = z$$

using chain rule  $\frac{dT}{dr} = \frac{dT}{dx} \cdot \frac{dx}{dr} + \frac{dT}{dy} \cdot \frac{dy}{dr}$

$$= \frac{dT}{dx} \cdot \cos \phi + \frac{dT}{dy} \cdot \sin \phi$$

$$\cos \phi \cdot \frac{dT}{dr} = \cos^2 \phi \cdot \frac{dT}{dx} + \sin \phi \cdot \cos \phi \cdot \frac{dT}{dy} \quad \text{--- (1)}$$

Also  $\frac{dT}{d\phi} = \frac{dT}{dx} \cdot \frac{dx}{d\phi} + \frac{dT}{dy} \cdot \frac{dy}{d\phi}$

$$= \frac{dT}{dx} \cdot (-r \sin \phi) + \frac{dT}{dy} \cdot (r \cos \phi)$$

$$\frac{\sin \phi}{r} \cdot \frac{dT}{d\phi} = -\sin^2 \phi \cdot \frac{dT}{dx} + \sin \phi \cdot \cos \phi \cdot \frac{dT}{dy} \quad \text{--- (2)}$$

From (1) & (2)

$$\frac{\sin \phi}{r} \cdot \frac{\partial t}{\partial \phi} = -\sin^2 \phi \frac{\partial t}{\partial x} + \left[ \cos \phi \cdot \frac{\partial t}{\partial r} - \cos^3 \phi \cdot \frac{\partial t}{\partial x} \right]$$

$$= -\frac{\partial t}{\partial x} + \cos \phi \cdot \frac{\partial t}{\partial r}$$

$$\frac{\partial t}{\partial x} = \cos \phi \cdot \frac{\partial t}{\partial r} - \frac{\sin \phi}{r} \cdot \frac{\partial t}{\partial \phi} \quad \text{--- (3)}$$

upon diff. with respect to  $x$ .

$$\frac{\partial}{\partial x} \left( \frac{\partial t}{\partial x} \right) = \frac{\partial}{\partial x} \left[ \cos \phi \cdot \frac{\partial t}{\partial r} - \frac{\sin \phi}{r} \cdot \frac{\partial t}{\partial \phi} \right]$$

$$\frac{\partial^2 t}{\partial x^2} = \cos \phi \cdot \frac{\partial}{\partial r} \left[ \frac{\partial t}{\partial x} \right] - \frac{\sin \phi}{r} \cdot \frac{\partial}{\partial \phi} \left[ \frac{\partial t}{\partial x} \right]$$

$$= \cos \phi \cdot \frac{\partial}{\partial r} \left[ \cos \phi \cdot \frac{\partial t}{\partial r} - \frac{\sin \phi}{r} \cdot \frac{\partial t}{\partial \phi} \right] - \frac{\sin \phi}{r} \cdot \frac{\partial}{\partial \phi} \left[ \cos \phi \cdot \frac{\partial t}{\partial r} - \frac{\sin \phi}{r} \cdot \frac{\partial t}{\partial \phi} \right]$$

$$\left[ \frac{\partial}{\partial r} \cdot \frac{1}{r} = -\frac{1}{r^2} \right]$$

$$\left[ \frac{\partial}{\partial \phi} \cdot \cos \phi = -\sin \phi \right] \quad \cos^2 \phi \cdot \frac{\partial^2 t}{\partial r^2} + \frac{\cos \phi \cdot \sin \phi}{r^2} \cdot \frac{\partial t}{\partial r} + \frac{\sin^2 \phi}{r} \cdot \frac{\partial t}{\partial \phi} +$$

$$\frac{\sin^2 \phi}{r^2} \cdot \frac{\partial t}{\partial r^2} + \frac{\sin \phi \cdot \cos \phi}{r^2} \cdot \frac{\partial t}{\partial \phi} \quad \text{--- (4)}$$

$$\text{Hence } \frac{\partial^2 t}{\partial y^2} = \sin^2 \phi \cdot \frac{\partial^2 t}{\partial r^2} + \frac{\cos^2 \phi}{r} \cdot \frac{\partial t}{\partial r} - \frac{\cos \phi \cdot \sin \phi}{r^2} \cdot \frac{\partial t}{\partial \phi} +$$

$$\frac{\cos^2 \phi}{r^2} \cdot \frac{\partial^2 t}{\partial r^2} - \frac{\cos \phi \cdot \sin \phi}{r^2} \cdot \frac{\partial t}{\partial \phi} \quad \text{--- (5)}$$

from (4) & (5)

$$\frac{\partial^2 t}{\partial x^2} + \frac{\partial^2 t}{\partial y^2} = \frac{\partial^2 t}{\partial r^2} + \frac{1}{r} \cdot \frac{\partial t}{\partial r} + \frac{1}{r^2} \cdot \frac{\partial^2 t}{\partial \phi^2} \quad \text{--- (6)}$$

Substituting (6) in  $\frac{\partial^2 t}{\partial x^2} + \frac{\partial^2 t}{\partial y^2} + \frac{\partial^2 t}{\partial z^2} + \frac{\rho g}{k} = \frac{1}{\alpha} \cdot \frac{\partial t}{\partial \tau}$



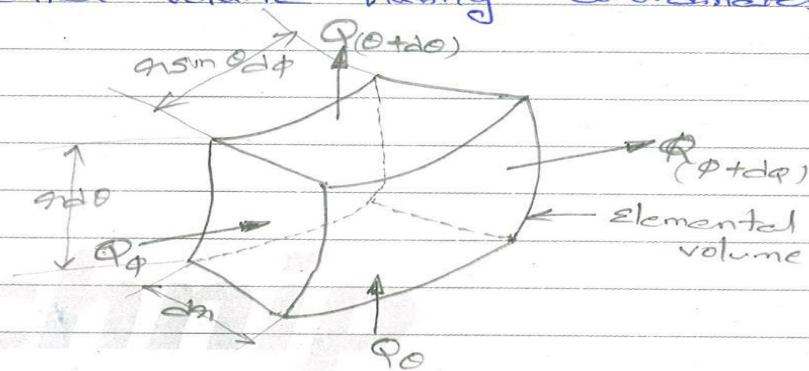
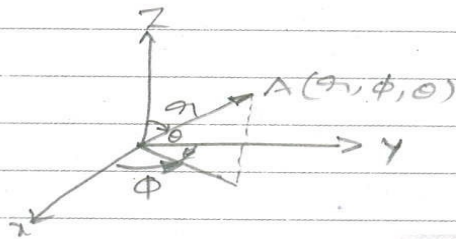
$$\left[ \frac{\partial^2 t}{\partial r^2} + \frac{1}{r} \cdot \frac{\partial t}{\partial r} + \frac{1}{r^2} \cdot \frac{\partial^2 t}{\partial \phi^2} + \frac{\partial^2 t}{\partial z^2} \right] + \frac{q_g}{k} = \frac{1}{\alpha} \cdot \frac{\partial t}{\partial \tau}$$

- For steady state uni-direction heat flow in the radial direction, and with no internal heat generation

$$\frac{\partial^2 t}{\partial r^2} + \frac{1}{r} \cdot \frac{\partial t}{\partial r} = 0$$

### → Spherical Co-ordinates:-

Consider an elemental volume having Co-ordinates  $(r, \phi, \theta)$ :



volume of the element =  $dr \cdot r d\theta \cdot r \sin\theta d\phi$

$q_g$  = heat generated per unit volume per unit time.

(i) Net heat accumulated in the element:-

Heat flow through  $r=0$  plane;  $\phi$ -direction;

net influx,  $Q_\phi = -k \cdot (dr \cdot r d\theta) \cdot \frac{\partial t}{r \sin\theta \cdot d\phi} \cdot dr$

Heat efflux,  $Q_{\phi+d\phi} = Q_\phi + \frac{\partial}{\partial \phi} (Q_\phi) \cdot r \sin\theta \cdot d\phi$

Heat accumulated in  $\phi$ -direction,

$$dQ_\phi = Q_\phi - Q_{\phi+d\phi}$$

$$= -\frac{1}{r \sin\theta} \cdot \frac{\partial}{\partial \phi} (Q_\phi) \cdot r \sin\theta \cdot d\phi$$

$$= \frac{-1}{r \sin \theta} \cdot \frac{\partial}{\partial \phi} \left[ -k \cdot (dr \cdot r d\theta) \frac{1}{r \sin \theta} \cdot \frac{\partial t}{\partial \phi} \cdot dr \right] \cdot r \sin \theta \cdot d\phi$$

$$= k \cdot [dr \cdot r d\theta \cdot r \sin \theta \cdot d\phi] \frac{1}{r^2 \sin^2 \theta} \cdot \frac{\partial^2 t}{\partial \phi^2} \cdot dr$$

Heat flow in  $r$ - $\phi$  plane,  $\theta$ -direction:

$$\text{Heat influx, } Q_\theta = -k \cdot (dr \cdot r \sin \theta d\phi) \cdot \frac{\partial t}{r \partial \theta} \cdot dr$$

$$\text{Heat efflux, } Q_{\theta+d\theta} = Q_\theta + \frac{\partial}{\partial \theta} (Q_\theta) r d\theta$$

Heat accumulated in  $\theta$ -direction:

$$dQ_\theta^* = Q_\theta - Q_{\theta+d\theta}$$

$$= -\frac{\partial}{\partial \theta} (Q_\theta) r d\theta$$

$$= -\frac{\partial}{\partial \theta} \left[ -k \cdot (dr \cdot r \sin \theta \cdot d\phi) \frac{\partial t}{r \partial \theta} \cdot dr \right] r \cdot d\theta$$

$$= \frac{k}{r} \cdot \frac{dr \cdot r d\phi \cdot r d\theta}{r} \cdot \frac{\partial}{\partial \theta} \left[ \sin \theta \cdot \frac{\partial t}{\partial \theta} \right] dr$$

$$= k \cdot dr \cdot r d\theta \cdot r \sin \theta \cdot d\phi \cdot \frac{1}{r^2 \sin \theta} \cdot \frac{\partial}{\partial \theta} \left[ \sin \theta \cdot \frac{\partial t}{\partial \theta} \right] dr$$

Heat flow in  $\theta$ - $\phi$  plane,  $r$ -direction:

$$\text{Heat influx } Q_r^* = -k \cdot (r d\theta \cdot r \sin \theta d\phi) \cdot \frac{\partial t}{\partial r} \cdot dr$$

$$\text{" efflux } Q_{r+dr} = Q_r + \frac{\partial}{\partial r} (Q_r) dr$$

Heat accumulated in  $r$ -direction:

$$dQ_r = Q_r - Q_{r+dr}$$

$$= -\frac{\partial}{\partial r} [Q_r] dr$$

$$= -\frac{\partial}{\partial r} \left[ -k \cdot (r d\theta \cdot r \sin \theta \cdot d\phi) \frac{\partial t}{\partial r} \cdot dr \right] dr$$

$$= k \cdot d\theta \cdot \sin \theta \cdot d\phi \cdot dr \cdot \frac{\partial}{\partial r} \left[ r^2 \cdot \frac{\partial t}{\partial r} \right] \cdot dr$$



Net heat accumulated in the element

$$= k \cdot dr \cdot r d\theta \cdot r \sin\theta \cdot d\phi \left[ \frac{1}{r^2 \sin^2\theta} \frac{\partial^2 t}{\partial \phi^2} + \frac{1}{r^2 \sin\theta} \frac{\partial}{\partial \theta} \left( \sin\theta \cdot \frac{\partial t}{\partial \theta} \right) + \frac{1}{r^2} \cdot \frac{\partial}{\partial r} \left( r^2 \cdot \frac{\partial t}{\partial r} \right) \right] dr$$

(ii) Heat generated within the element

$$= q_g \cdot (dr \cdot r d\theta \cdot r \sin\theta \cdot d\phi) dr$$

(iii) Energy stored in the element

The increase in thermal energy =  $S \cdot dr \cdot r d\theta \cdot r \sin\theta \cdot d\phi \cdot c \cdot \frac{\partial t}{\partial \tau} dr$   
from energy balance equation (1), (2), (3);

$$\textcircled{1} + \textcircled{2} = \textcircled{3} \quad ; \text{Dividing by } k \cdot [dr \cdot r d\theta \cdot r \sin\theta \cdot d\phi] dr,$$

$$\left[ \frac{1}{r^2 \sin^2\theta} \cdot \frac{\partial^2 t}{\partial \phi^2} + \frac{1}{r^2 \sin\theta} \cdot \frac{\partial}{\partial \theta} \left( \sin\theta \cdot \frac{\partial t}{\partial \theta} \right) + \frac{1}{r^2} \cdot \frac{\partial}{\partial r} \left( r^2 \cdot \frac{\partial t}{\partial r} \right) \right] + \frac{q_g}{k} = \frac{gc}{k} \cdot \frac{\partial t}{\partial \tau} = \frac{1}{\alpha} \cdot \frac{\partial t}{\partial \tau}$$

- For steady, one-D, no heat sources

$$\frac{1}{r^2} \cdot \frac{\partial}{\partial r} \left( r^2 \cdot \frac{\partial t}{\partial r} \right) = 0$$

The above equation can also be derived by using

$$x = r \sin\theta \cdot \sin\phi, \quad y = r \sin\theta \cdot \cos\phi, \quad z = r \cos\theta.$$